# CERTAIN QUESTIONS OF AEROTHERMODYNAMICS CONNECTED WITH THE MODEL OF <br> FREE-MOLECULAR FLOW 

# (NEKOTORYE VOPROSY AEROTEBMODINAMIKI, SVIAZANNYE S MODEL' IU SVOBODNOMOLERULIARNOGO POTOKA) 

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## n.t. PASHCHENKO <br> (Moscow)

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Heat exchange in very rarefied gases has been treated in a considerable number of papers. In [ 1,2] and a number of others, the question of determining the equilibrium temperature of a body (a flat plate or a cylinder) moving with constant velocity is considered. The body is assumed to be a perfect conductor and the total heat flow across its surface is calculated. Then, by virtue of the assumption of perfect conductivity, we avoid the unresolved questions connected with the unequal heating of surface elements which are differently oriented in relation to the velocity of motion. Moreover, as a result of it being a steady problem, we leave aside consideration of the process of establishing the temperatare equilibrium, which is well known to be important at great heights.

In the present paper, by making use of the expressions obtained in [3] for the heat transfer, we determine the temperature of a thin body which has small unsteady motions,* in addition to its forward velocity, both in the case of purely convective heat exchange and also in the case of radiative heat transfer. The temperature is determined as a function of time, local angle of attack, velocity, the characteristics of the

[^0]surface and the thermodynamic parameters of the medium at the height under consideration. We notice the important dependence of the time for establishing temperature equilibrium upon the height. For the assumed model of the interaction of the gas with the surface we find the temperature of the gas in contact with the surface and the temperature of the surface, and indicate the dependence of the temperature discontinuity between the gas and the wall upon the assumed model of interaction. We point out a certain similarity between the gasdynamic stagnation temperature and the equilibrium temperature of a plate in free-molecular flow. This fact, together with the similarity established in [3] between the expression for the excess pressure and the "piston theory" formula used in gasdynamics, may provide a certain basis for the application of the expressions obtained here to the temperature in the field of the mechanics of a continuous medium.

1. Let a body be moving through a highly rarefied gas with a constant velocity $V$ relative to a certain reference system fixed in space (the unperturbed velocity), and let it perform small unsteady motions relative to this unperturbed state. Then, according to the kinetic model of a gas assumed in [3], and under the limitations therein prescribed on the shape and motion of the body, we know that the heat transfer in time $d t$ to the surface element $d s$ is determined by the following expression:

$$
\begin{gather*}
\Delta Q=\frac{\varepsilon \rho_{\infty}}{2}\left\{\frac{2 R c^{\circ}}{\sqrt{\pi}}\left[T_{\infty}-T_{\infty}(1-\alpha)\left(1+\frac{2}{3} \frac{V^{\alpha} V^{\beta} g_{\alpha \beta}}{c^{\alpha}}\right)-\alpha T_{w}\right]+\right. \\
+\frac{c^{\circ}}{2 \sqrt{\pi}}\left[V^{\alpha} V^{\beta} g_{\alpha \beta}+2 V^{\alpha} w_{\cdot / t}^{\beta} g_{\alpha \beta}\right]+\frac{1}{2} V^{\alpha} V^{\beta} g_{\alpha \beta}\left(w_{\cdot / t}^{3}-V^{\gamma} w_{\cdot / 4}^{3}\right)+ \\
\left.+\frac{R}{2}\left[5 T_{\infty}-4 T_{\infty}(1-\alpha)\left(1+\frac{2}{3} \frac{V^{\alpha} V^{\beta} g_{\alpha \beta}}{c^{\circ} 2}\right)-4 x T_{w}\right]\left(w_{\cdot / t}^{3}-V^{\gamma} w_{\cdot / \gamma}^{3}\right)\right\} d s d t \tag{1.1}
\end{gather*}
$$

All tensor quantities are considered in coordinates related to the unperturbed constant velocity in the conventional manner. The following notation has been used: $\rho_{\infty}, T_{\infty}$ are the density and temperature of the incident medium, $c^{0}$ is the most likely velocity of random motion of the molecules, $w_{. / s}^{i}, w_{\cdot / t}^{i}$ are covariant derivatives of the components of the displacement vector with respect to the coordinates and time, $w_{\cdot / 3}^{3}=-1$, $R$ is the gas constant, $g_{a \beta}$ is the fundamental metric tensor of the coordinates under consideration, $a$ is the accommodation coefficient, $\epsilon$ is the coefficient of diffuse reflection, and $T_{w}$ is the temperature of the surface.

In determining the heating of the body let us take the following thermomechanical model. We shall assume that the layer of the rigid body next to $d s$ (henceforth this layer will be called the surface of the element or body) has a thickness $h$ sufficiently small so that we can assume that the mass included in the volume $h d s$ has a unifori temperature
$T$. The inner surface of the layer will moreover be assumed to be adiabatically insulated. Then into the volume $h$ ds under consideration there flows through $d s$ a quantity of heat $\Delta Q$ on account of the impacts with the gas molecules. Through the side faces there flows a quantity $\Delta Q_{1}$ on account of the heat conduction from the parts of the body imnediately surrounding $h \mathrm{ds}$. Through ds there is emitted a quantity of heat $\Delta Q_{2}$ on account of radiation (it is assumed that the surface radiates as a perfect black body according to the Stefan-Baltzmann law). Accordingly, the quantity of heat $\Delta Q_{3}$ used up in the heating of the surface element is determined from the condition of heat balance by the following expression:

$$
\begin{equation*}
\Delta Q_{s}=c \rho_{w} h d s d T_{w}, \quad \Delta Q_{s}=\Delta Q, \Delta Q_{1}-\Delta Q_{2} \tag{1.2}
\end{equation*}
$$

Here $c$ and $\rho_{0}$ are the specific heat capacity and the density of the body, respectively.

Let us express $\Delta Q_{1}$ and $\Delta Q_{2}$ by means of the parameters of the medium and the body. It is easy to see that

$$
\begin{equation*}
\Delta Q_{1}=k T_{w / \alpha \beta} g^{\alpha \beta} k d s d t \tag{1.3}
\end{equation*}
$$

where $k$ is the coefficient of thermal conductivity of the rigid body, $T_{w / a \beta} g^{a \beta}$ is the Laplace operator on the function $T_{v}$ in the coordinates under consideration

$$
\begin{equation*}
\Delta Q_{2}=\sigma T_{w}{ }^{4} d s d t \tag{1.4}
\end{equation*}
$$

and $\sigma$-is the Stefan-Boltzmann constant*.
Substituting (1.1), (1.3) and (1.4) into (1.2), we obtain, generally speaking, a nonlinear partial differential equation for the determination of the temperature $T_{w}$ of the surface as a function of the tiae $t$, the coordinates $x^{i}$, the properties of the surface, the characteristics of the motion of the body, and the thermodynamic parameters of the gaseous mediun at the height under consideration:

$$
\begin{aligned}
T_{w / t}= & \frac{k T_{w / \alpha \beta} g^{\alpha \beta}}{c \rho_{w}}+\frac{\varepsilon \rho_{\infty}}{2 c \rho_{w} h}\left\{\frac{2 R c^{\circ}}{\sqrt{\pi}}\left[T_{\infty}-T_{\infty}\left(1+\frac{2}{3} \frac{V^{\alpha} V^{\beta} g_{\alpha \beta}}{c^{\alpha}}\right)(1-\alpha)-\alpha T_{w}\right]+\right. \\
& +\frac{c^{\circ}}{2 \sqrt{\pi}}\left(V^{\alpha} V^{\beta} g_{\alpha \beta}+2 V^{\alpha} w \cdot / t g_{\alpha \beta}^{\beta}\right)+\frac{1}{2}\left(V^{\alpha} V^{\beta} g_{\alpha \beta}\right)\left(w . w^{3}-V^{\gamma} w \cdot / \gamma\right)+
\end{aligned}
$$

[^1]$$
\left.+\frac{R}{2}\left[5 T_{\infty}-4 T_{\infty}\left(1+\frac{2}{3} \frac{V^{\alpha} V^{\beta} g_{a \beta}}{c^{\circ}}\right)(1-\alpha)-4 \alpha T_{w}\right]\left(w_{\cdot / t}^{3}-V^{\gamma} w_{\cdot / \gamma}^{3}\right)\right\}-\frac{\sigma T_{w}^{4}}{c \rho_{w}^{h}}
$$

Questions related to the heat conduction along the surface will not be considered in this paper; as a result, the first term on the righthand side of Equation (1.5) is neglected. Accordingly, we exclude from consideration the thermal interaction of the parts of the body with each other. Then Equation (1.5) is transformed into an ordinary differential equation with respect to the anknown function $T_{v_{i}^{\prime}}$ where the time $t$ is the independent variable, and the coordinates $x^{i}$ are parameters. The displacement vector $w\left(x^{i}, t\right)$, characterizing the unsteady motion of the surface, is assumed to be a given function of the coordinates and time. Equation (1.5) can be put in the form

$$
\begin{equation*}
\frac{d T}{d t}=B_{1}-B_{2} T+B_{3}+B_{4}-B_{5} T^{4} \tag{1.6}
\end{equation*}
$$

Here we have introduced the following notation:

$$
\begin{gather*}
T=T_{w} / T_{\infty}, \quad V^{\alpha} V^{\beta} g_{\alpha \beta} / c^{\circ 2}=S^{2}, \quad \frac{w_{\cdot / t}^{3}-V^{\alpha} w_{\cdot / \alpha}^{3}}{c^{\alpha}}=S_{n}, \quad \frac{\varepsilon \rho_{\infty} R c^{o}}{c P_{w} h V \bar{\pi}}=a_{1}  \tag{1.7}\\
B_{1}=a_{1}\left[1-(1-\alpha)\left(1+\frac{2}{3} S^{2}\right)+\frac{S^{2}}{2}\right], \quad B_{2}=a_{1} \alpha\left[1+\sqrt{\pi} S_{n}\right], \quad B_{3}=a_{1} V^{\alpha} w_{\cdot / f}^{\beta} g_{\alpha \beta} / c^{o 8} \\
B_{4}=a_{1} \sqrt{\pi} S_{n}\left[\frac{1}{2} S^{2}+1.25-(1-\alpha)\left(1+\frac{2}{3} S^{2}\right)\right], \quad B_{5}=\frac{\sigma T_{\infty}^{3}}{P_{w c h}}
\end{gather*}
$$

Let us examine in some very simple particular problems the characteristic singularities of the phenomens which may arise in the assumed models of gas and body (we have in mind the kinetic model of a gas and the thermomechanical model of the body).
2. Let us consider the case of purely convective heat transfer (radiation absent). Equation (1.6) becomes linear

$$
\begin{equation*}
\frac{d T}{d t}=B_{1}-B_{2} T+B_{3}+B_{4} \tag{2.1}
\end{equation*}
$$

and its general solution is given by the formula

$$
\begin{equation*}
T=\exp \left(-\int_{0}^{t} B_{2} d t\right)\left[T_{00}+\int_{0}^{t}\left(B_{1}+B_{3}+B_{4}\right) \exp \left(\int_{0}^{x} B_{2} d x\right) d t \quad\left(T_{00}=\frac{T_{w_{0}}}{T}\right)\right. \tag{2.2}
\end{equation*}
$$

Where $T_{00}$ is the dimensionless initial temperature of the elenent of the surface.

Let the body perfori only the unperturbed motion, then the $B_{i}$ do not depend on time, and the general solution in this case with $B_{2} \neq 0$ has the
form*

$$
T=T_{00} \exp \left(-B_{2} t\right)+\left[1-\exp \left(-B_{2} t\right)\right] \frac{\left(B_{1}+B_{3}+B_{4}\right)}{B_{2}}
$$

or, substituting for the $B_{i}$ their expressions, introducing the local angle of attack $\beta$ and replacing $S$ by its value

$$
S=\sqrt{1 / 2 x} M
$$

we obtain

$$
\begin{align*}
T= & T_{00} \exp \left[-a_{1} \alpha t(1+\sqrt{x \pi / 2} M \beta)\right]+\frac{1}{\alpha}\left\{1+(1-\alpha)\left(1+\frac{x M^{2}}{3}\right)+\right. \\
& \left.+\frac{x M^{2}}{4}+\frac{\sqrt{\kappa \pi / 2} M \beta}{4(1+\sqrt{x \pi / 2} M \beta)}\right\}\left\{1-\exp \left[-a_{1} \alpha t(1+\sqrt{x \pi / 2} M \beta)\right]\right\} \tag{2.3}
\end{align*}
$$

Hence, when $t \rightarrow \infty$ we find an asymptotically attained dimensionless equilibrium temperature

$$
\begin{equation*}
T_{e}=\frac{1}{\alpha}\left[1+(1-\alpha)\left(1+\frac{x M^{2}}{3}\right)+\frac{x M^{2}}{4}+\frac{\sqrt{x \pi / 2} M \beta}{4(1+\sqrt{x \pi / 2} M \beta)}\right] \tag{2.4}
\end{equation*}
$$

On a plate, moving with zero angle of attack, with $a=1$ the equilibrium temperature becomes

$$
\begin{equation*}
T_{e}=1+\frac{x M^{2}}{4} \tag{2.5}
\end{equation*}
$$

According to the restrictions postulated in [3] on the shape and motion of the body ( $S_{n} \ll 1$ ), the singularities in Expressions (2.3), (2.4) occur outside the limits of applicability of the expression for the heat transfer in the form (1.1) (the appearance of the singularity is a result of introducing the inearization in [3]). The presence of the singularity may serve as a certain indication of the liaits of applicable values of $M \beta$.

Let us consider the steady temperature as a function of the local angle of attack. It is easy to see that the temperature of the parts of the surface turned towards the stream are higher than the temperature

[^2]attained on the flat plate, Let us find the difference in the equilibrium temperatures $\Delta T_{e}$ for two elements of the surface inclined at angles $\beta$ and $-\beta$ with respect to the direction of the velocity of the incident stream:
\[

$$
\begin{equation*}
\Delta T_{e}=\frac{M \beta}{2 \alpha} \sqrt{\frac{\chi \pi}{2}} \frac{1}{1-\chi \pi / 2 M^{2} \beta^{2}} \tag{2.6}
\end{equation*}
$$

\]

Calculations carried out for a number of values of $\mu$ and $\beta$ show that the difference of temperature at the points of the surface under consideration consists, as a rule, of a small percentage of the corresponding temperature of the flat plate at zero angle of attack, at least in the region of permissible values of $M \beta$ (obviousiy, with increase in $M$ the permissible values of the angle of attack $\beta$ diminish). However, it can be shown that allowance for this difference of temperature is important in the determination of thermal stresses arising in structures.

In [1,2] only the equilibrium temperature is determined, which does not depend on the height, as is clear from (2.4). It must be remarked, however, as calculations from Formula (3) show, that at the greatest heights ( $\approx 100 \mathrm{~km}$ and higher) the process of establishing the equilibrium temperature occurs very slowly. This can be seen in the table and Fig.1, where the broken curves show the variation of the temperature $T_{1}$ of the body without allowance for radiation, and the full curves show the temperature $T_{2}$ of the body with allowance for radiation. So, for example, in the motion of a body at zero angle of attack at heights of $150-200 \mathrm{~km}$ with dimensionless velocity $S=20$ for a period of $21 / 2$ hours the temperature of the surface remains practically equal to the initial temperature. Notwithstanding the fact that in the absence of radiation the equilibrium temperature does not depend on height, the time taken to establish this temperature is considerably influenced by the height.

Let us consider the expression for the equilibrinm temperature set up on a flat plate (2.5). From boundary-layer theory it is known [4] that in the flow of a steady stream of compressible gas with Prandtl number equal to unity past a plate, with the so-called "adiabatic wall" as the temperature boundary condition (it is assumed that the temperature of the gas at the surface of the plate is equal to the temperature of the plate), there exists an integral of the equation of energy, the StodolaCrocco integral, which may be written for dimensionless temperatures in the form

$$
\begin{equation*}
T_{e}^{*}=1+\frac{1}{2}(x-1) M^{2} \tag{2.7}
\end{equation*}
$$

It is not difficult to show the similarity of the equilibrium temperature (2.5) obtained in the case under consideration with the StodolaCrocco integral. Comparing (2.5) and (2.7), we can see that when $a=1$
these expressions differ only by the factor involving $\kappa$, and they coincide when $\kappa=2$. When $\kappa<2$ the equilibrium temperature (2.6), established on the flat plate with free-molecular flow, is higher than the corresponding stagnation temperature (2.7) of continuous flow, which is found in accordance with the results of [2], but not higher than the kinetic temperature * $T_{k}=1+K M^{2} / 3$ of the free-molecular flow with mass velocity $V$.

In the general case $a \neq 0$ the equilibrium temperature (2.4) established on the surface depends upon the magnitude of $a ; a=0$ is a special case, when the body receives heat but does not give it up, as a result of which the temperature increases without 1 imit and, as is evident from (2.2), there does not exist a steady bounded solution of the problem.

The boundary-layer condition on the surface temperature (equality of the temperature of the surface and of the gas in contact with the surface) is not the only one applicable to the stated problem, and it cannot always apply. Thus, the assumed model of interaction of the molecules of the gas with the surface already determines the value of the temperature of the gas in contact with the wall, which is different from the equilibrium temperature $T_{e}$ established on the surface itself (2.4). The dimensionless temperature $T^{\circ}$ of the gas in contact with the surface of the body, obtained by means of the boundary value of the distribution function ([3], Formula (1.1)), is given by

$$
\begin{align*}
T^{\circ}=\alpha \varepsilon T & +\left[\frac{2-\varepsilon}{2}\left(1+\frac{\chi M^{2}}{3}\right)\left(1+\sqrt{\frac{\chi}{2 \pi}} M \beta\right)\right]+ \\
& +\frac{\varepsilon}{2}\left[\left(1+\frac{\chi M^{2}}{3}\right)(1-\alpha)-\alpha T\right] \tag{2.8}
\end{align*}
$$

In the case of the commonly accepted value of the accommodation coefficient $a=1$, Expression (2.7) has the form

$$
\begin{equation*}
T^{\circ}=\varepsilon T+\frac{2-\varepsilon}{2}\left[\left(1+\frac{x M^{2}}{3}\right)\left(1+\sqrt{\frac{x}{2 \pi}} M \beta\right)\right]-\frac{\varepsilon T}{2} \tag{2.9}
\end{equation*}
$$

Accordingly, the model is such that the temperature of the gas in contact with the wall depends upon the kinetic temperature of the gas,

* The kinetic temperature of a gas is found [5] from the relation

$$
\left.\frac{3}{2} R T_{k}=\int_{\Omega} c^{i} c_{i} f \mathrm{~d} c \right\rvert\, \int_{\Omega} f \mathrm{~d} c
$$

( $\Omega$ is the region of integration, $0<|c|<\infty$ ) in the given case $f$ is the Maxwell distribution with mass velocity $V$.
the temperature of the wall, its shape and the nature of the interaction of the molecules with the surface.

Let us consider a particular case of the interaction of the molecules with the surface. With pure specular reflection ( $\epsilon=0$ ) the temperature of the gas in contact with the wall does not depend on the temperature of the wall

$$
T^{\circ}=\left(1+\frac{1}{3} x M^{2}\right)\left(1+\sqrt{\frac{x}{2 \pi}} M \beta\right)
$$

and in the case of a flat plate is equal to the kinetic temperature of the gas. In the case of pure diffusive reflection ( $\epsilon=1$ )

$$
\begin{equation*}
T^{\circ}=T+\frac{1}{2}\left[\left(1+\frac{1}{3} x M^{2}\right)\left(1+\sqrt{\frac{x}{2 \pi}} M \beta\right)-T\right] \tag{2.10}
\end{equation*}
$$

and for a flat plate, moving at zero angle of attack, we obtain (with $a=1$ )

$$
\begin{equation*}
T^{\circ}=T+\frac{1}{2}\left(1+\frac{1}{3} x M^{2}-T\right) \tag{2.11}
\end{equation*}
$$

Frow (2.11) we can see that $T^{\circ}<T$ if the surface possesses a temperature higher than the sinetic temperature of the gas, and vice versa. Accordingly, generally speaking, at the contact surface of the gas with the surface (within the assumptions of the accepted model of the gas, the surface and their interaction) there exists a discontinuity of temperature, and only in the special case when the flat plate warms up to the kinetic temperature of the stream does the temperature of the gas in contact with the flat plate equal the temperature of the plate itself. Moreover, this temperature is different from the equilibrium temperature, set up in the plate as a result of only convective heat transfer.

Expression (2.8) for the temperature of the gas in contact with the wall can be used as a boundary condition in the solution of temperature problews in the gas.
3. Let us consider heat transfer with radiation. In the case of unperturbed motion of the surface the $B_{i}$ do not vary with time, the variables in the equation (1.6) are separated, and its solution can be obtained in quadratures

$$
\begin{equation*}
t=\int_{\gamma_{\infty}}^{T} \frac{d T}{B_{1}-B_{2} T+B_{3}+B_{4}-B_{5} T^{4}} \tag{3.1}
\end{equation*}
$$

Calculations which have been carried out show (Fig. 1 and the table) that at the greatest heights ( 150 km and higher) radiation plays a
fundamental part in heat transfer from the surface to the medium. If we take for the initial temperature the temperature of the surrounding

Dependence of dimensionless temperature
on time with $a=1, \epsilon=0, S=20$, $c=0.12 \mathrm{cal} . \mathrm{cm} \mathrm{g}^{-1} \mathrm{deg}^{-1}$, $\rho_{v}=7.9 \mathrm{~g} \mathrm{~cm}^{-3}, h=0.5 \mathrm{~cm}$.


Fig. 1.

| $H, F_{\infty} T_{\infty}$ | $t$ | $T_{1}$ | $T_{2}$ |
| :---: | :---: | :---: | :---: |
| $\begin{gathered} H=100 \mathrm{~km} \\ \rho_{\infty}=0.829 \cdot 10^{-\theta} \mathrm{g} \mathrm{~cm}^{-3} \\ T_{\infty}=237^{\circ} \mathrm{K} \end{gathered}$ | 10 | 1.28 | 1.27594 |
|  | 20 | 1.6 | 1.51412 |
|  | 30 | 1.8 | 1.69201 |
|  | 40 | 2.196 | 1.80242 |
|  | 50 | 2.396 | 1.8587 |
|  | 60 | 2.792 |  |
|  | $\infty$ | 201 | 1.889 |
| $\begin{gathered} H=150 \mathrm{~km} \\ \rho_{\infty}=0.34 \cdot 10^{-11} \mathrm{~g} \mathrm{~cm} \\ T_{\infty}=418^{\circ} \mathrm{K} \end{gathered}$ | 10 | 1.002 | 0.87623 |
|  | 20 | 1.004 | 0.80394 |
|  | 30 | 1.006 | 0.75319 |
|  | 40 |  | 0.71447 |
|  | 50 | 1.008 | 0.68343 |
|  | 60 | 1.00995 | 0.65773 |
|  | 70 | 1.012 | 0.6359 |
|  | 80 | 1.014 | 0.61703 |
|  | 90 | 1.0146 | 0.60049 |
|  | 100 | 1.016 | 0.58572 |
|  | 110 | 1.018 | 0.57269 |
|  | 120 | 1.02 | 0.56058 |
|  | 130 | 1.022 | 0.55007 |
|  | 140 | 1.024 | 0.54022 |
|  | 150 | 1.026 |  |
|  | $\infty$ | 201 | 0.328 |
| $\begin{gathered} H=200^{\mathrm{km}} \\ \mathrm{P}_{\infty}=0.166 \cdot 10^{-12} \mathrm{~g} \mathrm{~cm}^{-3} \\ T_{\infty}=647^{\circ} \mathrm{K} \end{gathered}$ | 10 | 1.00091 | 0.53505 |
|  | 20 | 1.002 | 0.49705 |
|  | 30 | 1.0028 | 0.46875 |
|  | 40 | 1.0038 | 0.4464 |
|  | 50 | 1.0048 | 0.42303 |
|  | 60 | 1.0058 | 0.41252 |
|  | 70 | 1.0068 | 0.39915 |
|  | 80 | 1.0076 | 0.38745 |
|  | 90 | 1.0086 | 0.35997 |
|  | 100 | 1.0096 | 0.33954 |
|  | 110 | 1.0106 |  |
|  | 120 | 1.0116 |  |
|  | 130 | 1.0124 |  |
|  | 140 | 1.0134 |  |
|  | 150 | 1.0144 |  |
|  | $\infty$ | 201 | 0.121 |

medium, then, as is evident from Fig. 1 , the equilibrium temperature in the presence of radiation heat transfer, beginning at a height of 150 $k m$, is lower than the temperature of the surrounding medium and much lower than the equilibriun tempersture found in a calculation taking
account only of purely convective heat transfer.
And here, as also in the preceding case (Section 2), it is necessary to pay attention to the duration of the process of establishing the equilibrium temperature. The variation of the temperature with time for different heights was obtained by numerical integration of Equation (1,6), the thermodynamic characteristics of the medium at different heights being obtained from [6,7]. In the calculations the surface was taken to have the following characteristics: $\epsilon=1, a=1$, $c=0.12 \mathrm{cal} . \mathrm{g}^{-1} \mathrm{~cm}^{-3} \mathrm{deg}^{-1}, \rho=$ $7.9 \mathrm{~g} \mathrm{~cm}^{-3}, h=0.5 \mathrm{~cm}$.
4. The results obtained in this paper, generally speaking, are valid only for great heights in the region of free-molecular flow. We have already noticed the analogy established


Fig. 2. in [3] between the pressure in freemolecular flow and the flow of an ideal compressible fluid. Comparison of Formulas (2.7) and (2.5) of the present paper allows us to perceive a similar analogy with regard to temperatures. Since in the mechanics of a continuous medium we have still not discovered a simple relation between


Fig. 3. the temperature of the surface or the heat intake and the local angle of attack in unsteady motion, there is some interest, in view of the specified analogy, in assuming (op to the present time, we have failed to obtain the rigorously proved dependence of temperature and heat intake on the local angle of attack) as a hypothesis for the gasdynamic calculations the expression obtained in form (1.1) for the heat intake and all the consequences arising therefrom.

Computations were carried out for the deterwination of temperature at heights $20-50 \mathrm{~km}$, both in the case of purely conductive heat transfer, and also for heat transfer with radiation when $S=5$. The results show that with decrease of height the part played by radiation in the
overall heat balance decreases (we must not, however, forget that in this problem we have considered only the radiation of the surface itself, and have not taken into account the influence of radiation of the gas). In Figs. 2 and 3 are shown the variation with time of the temperature of the bods $T_{1}$ without allowing for radiation, and $T_{2}$ with allowance for radiation. Figure 2 shows the process of establishing the equilibrium temperature at a height of 20 km , and Fig. 3 at a height of $50 \mathrm{~km} . T_{\text {el }}$ and $T_{e}$ denote the equilibrium temperatures in the absence and presence of radiation, respectively. From the graphs it is clear that as the height decreases the process of establishing the equilibrium temperature proceeds significantly faster. In the graphs we can also see the influence of the angle of attack on the process of establishing the equilibrian temperature.

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[^0]:    - A similar study can be carried out for the determination of the temperature of the surface of thick convex bodies in steady motion, but instead of Expression (1.1) of the present paper we need to use the corresponding expression for the heat transfer derived, for example, in [1,2].

[^1]:    - In the case when the body is not perfectly black, we have to attach to the right-hand side of the equation a factor characterizing the degree of blackness.

[^2]:    * The case $B_{2}=0$, according to the meaning of the quantities determining $B_{2}(1.7)$, can occur either when $a=0$ or when $\epsilon=0$. The first case corresponds to heat transfer being independent of the temperature of the surface, and it leads, as is apparent from (2.2), to a linear increase with time of the temperature of the surface. In the case $\epsilon=0$ the heat transfer to the surface is zero and for the whole duration of the motion the temperature remains equal to its initial value.

